

CBGS SCHEME

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21AU51

Fifth Semester B.E. Degree Examination, Dec.2023/Jan.2024 Heat and Mass Transfer

Time: 3 hrs.

Max. Marks: 100

Note: 1. Answer any FIVE full questions, choosing ONE full question from each module.
2. Use of Thermodynamics, Heat transfer Data hand book is permitted.

Module-1

- 1 a. Discuss the three basic modes of heat transfer. Write the governing equations for the same and the governing laws. (12 Marks)
- b. The heat flow rate across an insulating material of thickness 30 mm with thermal conductivity $0.1 \text{ W/m}^\circ\text{C}$ is 250 W/m^2 . If the hot surface is 175°C , find the temperature of the cold surface. (08 Marks)

OR

- 2 a. Derive one dimensional heat conduction equation for rectangular or Cartesian co-ordinates, in differential form. (10 Marks)
- b. An aircraft heat exchanger has a maximum wall temperature of 810 K . The hot and cold side heat transfer coefficients are respectively $200 \text{ W/m}^2\text{K}$ and $400 \text{ W/m}^2\text{K}$. Find the maximum possible unit thermal resistance per m^2 area of the metallic wall separating the hot gas from the cold gas, if the hot gas temperature is 1200 K and the coolant temperature is 300 K . (10 Marks)

Module-2

- 3 a. Define :
- (i) Fin efficiency
- (ii) Fin effectiveness using the basic definition, arrive at the efficiency for,
- a long fin of rectangular cross section
 - rectangular fin with insulated tip. (10 Marks)
- b. Calculate the heat loss rate from a rectangular fin surface on a plane wall. The fin is 20 mm long, the breadth and thickness being 200 mm and 2 mm respectively. Assume negligible heat loss from the fin tip. Take $\theta_0 = 200^\circ\text{C}$, $h = 15 \text{ W/m}^2\text{K}$ and $K = 45 \text{ W/mK}$. (10 Marks)

OR

- 4 a. Show that the temperature history of a cooling body with negligible internal resistance is given by, $\frac{\theta}{\theta_0} = e^{\left(\frac{-hA}{\rho C_p V}\right)t}$. (10 Marks)
- b. A ball of 60 mm diameter at 600°C is suddenly immersed in controlled medium at 100°C . Calculate the time required for the ball to obtain a temperature of 150°C . Assume $K = 40 \text{ W/mK}$, $\rho = 800 \text{ kg/m}^3$, $C_p = 500 \text{ J/kgK}$, $h = 20 \text{ W/m}^2\text{K}$ for the ball. (10 Marks)

Module-3

- 5 a. Using dimensional analysis, show that $Nu = f(Gr, Pr)$ for natural convection. (12 Marks)
- b. Find the heat loss from both sides of a hot square plate $50 \text{ cm} \times 50 \text{ cm}$ at 100°C , exposed to atmosphere at 20°C , if the plate is kept vertical. Use the following relation.

$$Nu = 0.13(Gr.Pr)^{\frac{1}{3}} \rightarrow \text{vertical position at } 60^\circ\text{C, take } \rho = 1.06 \text{ kg/m}^3, K = 0.028 \text{ W/mK}$$

$$\gamma = 18.97 \times 10^{-6} \text{ m}^2/\text{s}, C_p = 1.008 \text{ kJ/kg-K} :$$

(08 Marks)

OR

- 6 a. Define the following dimensionless numbers and mention their significance, writing relevant equations:
- Prandtl number
 - Reynolds number
 - Nusselt number
 - Stanton number
- (10 Marks)
- b. Air at 27°C is moving at 0.3 m/s across a 100 W electric bulb at 127°C. If the bulb is approximated by a 10 cm diameter and 1 m high cylinder, estimate the heat transfer rate and percentage of power lost due to convection. At 77°C, take $Pr = 0.697$, $k = 0.03 \text{ W/mK}$, $\gamma = 2.08 \times 10^{-5} \text{ m}^2/\text{s}$.
- (10 Marks)

Module-4

- 7 a. Derive an expression for LMTD for a parallel flow heat exchanger. State the assumptions made. (10 Marks)
- b. A heat exchanger is required to cool 55000 kg/h of alcohol from 66°C to 40°C using 40000 kg/h of water entering at 5°C. Assuming parallel flow, calculate
- the exit temperature of water
 - heat transfer
 - surface area required.
- Take $u = 580 \text{ W/m}^2\text{K}$, $C_p(\text{alcohol}) = 3760 \text{ J/kgK}$, $C_p(\text{water}) = 4180 \text{ J/kgK}$. (10 Marks)

OR

- 8 a. Sketch and explain different regimes of boiling mechanism. (10 Marks)
- b. Air free saturated steam at 85°C and pressure of 57.8 kPa condenses on the outer surface of 225 horizontal tubes of 1.27 cm OD arranged in a 15×15 array. Tube surface is maintained at 75°C. Find the total condensation rate per m length of the tube bundle.

$$\text{Take : } h_m = 0.725 \left[\frac{g \rho_1^2 h_{fg} K_c^3}{\mu_1 (T_v - T_w) DN} \right]$$

where N = Number of tubes ; D = Tube diameter,

Physical properties of water at film temperature of 80°C , $K_1 = 0.668 \text{ W/m}^2\text{C}$,

$\mu_1 = 0.355 \times 10^{-3} \text{ kg/m-s}$, $h_{fg} = 2309 \text{ kJ/kg}$, $\rho_1 = 974 \text{ kg/m}^3$.

(10 Marks)

Module-5

- 9 a. Define the following laws of radiation, write appropriate relations. Discuss both of them :
- Stefan-Boltzman law
 - Kirchoff's law.
- (12 Marks)
- b. Assuming the sun to be a black body, calculate the surface temperature of the sun and emissive power of the sun's surface. Determine the maximum monochromatic emissive power, taking maximum radiation intensity from sun at $\lambda = 0.52 \mu$. (08 Marks)

OR

- 10 a. Define :
- Intensity of radiation
 - Solid angle
 - Lambert's law.
- (12 Marks)
- b. Two large parallel plates are at 1000 K and 800 K. Determine the heat exchange per unit area when (i) The surfaces are black (ii) The hot surface has an emissivity of 0.9 and cold, 0.6. (08 Marks)

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